PATENT COOPERATION TREATY

PCT

REC'D 08 MAR 2005

WIPO

PCT

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

(Chapter II of the Patent Cooperation Treaty)

(PCT Article 36 and Rule 70)

| Applicant's or agent's file reference | FOR FURTHER ACTION | See Form P | CT/IPEA/416 |
|--|--|---|---|
| P1897PC00 International application No. International filing date (a | | month/year) | Priority date (day/month/year) |
| Mitchiational applications of the second sec | | | 27.11.2003 |
| PCT/FI2004/000713 International Patent Classification (IPC) | | | |
| | | | |
| See Supplemental Box | | | |
| | | | |
| Applicant | | | |
| Fortum OYJ et al | | | |
| 1. This report is the international p | oreliminary examination report, e transmitted to the applicant acco | established by the ording to Article | is International Preliminary Examining 36. |
| | | luding this cove | er sheet. |
| | | | |
| | | | • Calleren |
| a. (sent to the applica | ant and to the International Bure | au) a total of | sheets, as follows: |
| and/or shee | ets containing rectifications authorities Instructions). | orized by this Authorities Author | we been amended and are the basis of this report uthority (see Rule 70.16 and Section 607 of the prity considers contain an amendment that goes as indicated in item 4 of Box No. I and the |
| Supplemen | ntal Box. | | ed, as indicated in item 4 of Box No. I and the |
| b. sent to the Interne | ational Bureau only) a total of (ii | ndicate type and | number of electronic carrier(s)) |
| | , containing a | a sequence listing to Sequence | g and/or tables related thereto, in electronic ence Listing (see Section 802 of the |
| form only, as indi- Administrative In | cated in the Supplemental Box it structions). | Clating to boda. | |
| | as relating to the following items: | • | |
| _ | is of the report | | |
| | ority | | |
| | • | regard to novelty | y, inventive step and industrial applicability |
| | k of unity of invention | _ | |
| | | 5(2) with regard | to novelty, inventive step or industrial |
| Box No. V Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement | | | |
| • | tain documents cited | | |
| Box No. VII Certain defects in the international application | | | |
| Box No. VIII Certain observations on the international application | | | n |
| | | | |
| Date of submission of the demand | | Date of completi | ion of this report |
| | | | |
| 20.06.2005 | | 10-02-20 | 06 |
| Name and mailing address of the IPE | EA/SE | Authorized office | cer |
| Patent- och registreringsver | | | |
| Box 5055 S-102 42 STOCKHOLM | | Moa Grönkvist/EÖ | |
| Facsimile No. +46 8 667 72 | 88 | Telephone No. | +46 8 782 25 00 |

International application No.

PCT/FI2004/000713

In case the space in any of the preceding boxes is not sufficient.

Continuation of: Cover sheet

INTERNATIONAL PATENT CLASSIFICATION (IPC):

B01J 23/40 (2006.01)

Form PCT/IPEA/409 (Supplemental Box) (April 2005)

International application No.

PCT/FI2004/000713

| Box | No. I | Basis | of the report | | |
|-----|---|----------------------|--|--|--|
| | | | e language, this report is based on: | | |
| 1. | | | | | |
| | the international application in the language in which it was filed a translation of the international application into | | | | |
| | which is the language of a translation furnished for the purposes of: | | | | |
| | | | nternational search (Rules 12.3(a) and 23.1(b)) | | |
| | | | publication of the international application (Rule 12.4(a)) | | |
| | | <u></u> | nternational preliminary examination (Rules 55.2(a) and/or 55.3(a)) | | |
| 2. | furnish | ed to the i | the elements of the international application, this report is based on (replacement sheets which have been receiving Office in response to an invitation under Article 14 are referred to in this report as "originally filed" exed to this report): | | |
| | | | national application as originally filed/furnished | | |
| | | the descr | ription: | | |
| | | pages _ | as originally filed/furnished | | |
| | | pages* _ | received by this Authority on received by this Authority on | | |
| | | pages*_ | received by this Addronty on | | |
| | \boxtimes | the claim | ns: as originally filed/furnished | | |
| | | pages | as amended (together with any statement) under Article 19 | | |
| | | pages* | 1-3 received by this Authority on 16-01-2006 | | |
| | | pages* | 1 I has this Anthority on | | |
| | \boxtimes | the draw | wings: | | |
| | E3 | pages | 1-2 as originally filed/furnished | | |
| | | pages* | - in Anthority on | | |
| | | pages* | ence listing and/or any related table(s) – see Supplemental Box Relating to Sequence Listing. | | |
| | | a seque | ince listing and/or any related table(s) — see supplemental 2011 - constant 2011 | | |
| 3 | . 🛛 | The am | nendments have resulted in the cancellation of: | | |
| | | | the description, pages | | |
| | | | the claims, Nos. 1-7 | | |
| | | | the drawings, sheets/figs | | |
| 1 | | 吕 | the sequence listing (specify): | | |
| | | | any table(s) related to the sequence listing (specify): | | |
| 1 | 4. | This remade, 70.2(c) | report has been established as if (some of) the amendments annexed to this report and listed below had not been since they have been considered to go beyond the disclosure as filed, as indicated in the Supplemental Box (Rule c)). | | |
| | • | | the description, pages | | |
| | | | the claims, Nos. | | |
| | | | the drawings, sheets/figs | | |
| | | | the sequence listing (specify): | | |
| | | | any table(s) related to the sequence listing (specify): | | |
| | * If it | tem 4 appl | lies, some or all of those sheets may be marked "superseded." | | |

International application No.

PCT/FI2004/000713

| Box N | Vo. V | Reasoned statement un citations and explanati | | 35(2) with regard to novelty, inventive step or industrial applicabiling such statement | ity; |
|-------|-----------|---|------------------|---|-----------|
| 1. S | Statement | | | | |
| | Novel | ty (N) | Claims Claims | 1-16 | YES NO |
| | Invent | ive step (IS) | Claims Claims | 1-16 | YES NO |
| | Indust | rial applicability (IA) | Claims Claims | | YES NO |

2. Citations and explanations (Rule 70.7)

Reference is made to the following documents:

D1: US2001048970

D2: W09110510

D3:Lashdaf M. et.al., Deposition of palladium and ruthenium beta-diketonates on alumina and silica supports in gas and liquid phase, Applied Catalysis A 241, 51-63 (2003)

D4: Dossi C. et.al., Chemical vapor deposition of platinum hexafluoroacetyalacetonate inside KL Zeolite: A new route to nonacidic platinum-in-zeolite catalysts, Journal of catalysis 145, 377-383 (1994)

D5: US6235962 D6: WO0040676 D7: WO0208156

The invention relates to a method for producing a nobel metal catalyst comprising the steps of pre-treating a zeolite with medium or large pore size, deposition of a nobel metal by gas phase deposition and a heat treatment. The nobel metals used in the production are platinum, palladium, ruthenium, rhodium, iridium and mixtures thereof. The invention relates to the use of said catalyst and production of a middle distillate diesel fuel.

Document D1 relates to a method for producing Pd/Au shell catalysts by chemical vacuum deposition, CVD (see section 19). As supports, it is possible to use inert materials such as SiO2, Al2O3, TiO2, ZrO2, MgO or mixtures of SiC and Si3N4 (see claim 4).

Document D2 relates to the use of saturating gas-solid

International application No.

PCT/FI2004/000713

Supplemental Box

In case the space in any of the preceding boxes is not sufficient.

Continuation of: Box V

reactions in a gas phase process, for the manufacture of a heterogeneous catalyst. The main groups of catalysts are represented by zeolite supported zinc, alumina-supported rhenium and silica supported chromium. The process comprises an optional pre-treatment step wherein the support is heated (see claim 6). Then the surface activated support is contacted and allowed to interact with vapour containing the catalytically active species or its precursor, then optional after-treatment follows (see claim 1).

Document D3 relates gas solid reactions for the deposition of vaporised Pd and Ru beta-diketonates on alumina and silica supports (see section 2.1). The metals are deposited on a preheated support with nitrogen as carrier gas. After deposition the samples are reduced.

Document D4 relates to the decomposition of volatile organometallic precursors inside zeolites. Pt/KL catalysts are prepared from platinum hexafluoro acetylacetonate precursors (see Catalyst preparation). The support is pre-heated and the deposition is performed in a flow of argon. Subsequent decomposition is also performed.

Document D5 relates to heterogenous catalysts for ring-opening reactions of cyclic organic compounds such as naphtalene present in diesel fuel. The catalyst comprises catalytically active metal such as platinum on a carrier of alumina, silica or zirconia (see column 2, line 1-38). The hydrocarbons are introduced in a reactor under a pressure of 1 to 100 atm and a temperature from 450 to 670 K (see column 2, line 24-34).

Document D6 relates to the production of diesel fuel by ringopening of naphthalene. Platinum on large pore crystalline zeolite (e.g. morderite) supports is used (see page 5, line 1-16 and page 6, line 10-16). Pressure ranges will vary from 400 to 1000 psi, and reaction temperatures will range from 288 to 370 C depending on the feedstock (see page 5, line 17-26).

.../...

International application No.

PCT/FI2004/000713

Supplemental Box

In case the space in any of the preceding boxes is not sufficient.

Continuation of: Box V

Document D7 relates naphthalene ring-opening catalysts comprising metals, such as platinum supported on inorganic oxides such as alumina or silica (see section 0025 and 0026). Preferred process conditions include temperatures from 150 C to 400 C and pressures from 100 to 3000 psi (see section 0029).

D2 is considered to be the closest prior art.

The method for manufacturing a catalyst according to claim 8 differs from D2 in that the nobel metals platinum, palladium, ruthenium, rhodium, iridium and mixtures thereof is used in the production. The problem to be solved by the present invention may therefore be regarded as producing a catalyst with high selectivity for ring-opening reactions. No teaching of specific catalysts that promote ring-opening reactions is suggested in D2 and non of the above mentioned nobel metals are suggested.

Therefore, claim 1 is considered to involve an inventive step. The use of said catalyst according to claim 15 and the production of a middle distillate diesel fuel in the presence of said catalyst according to claim 16 are also considered to involve an inventive step in view of the cited documents.

Accordingly, the invention defined in claims 1-16 is novel and is considered to involve an inventive step. The invention is industrially applicable.

International application No.

PCT/FI2004/000713

| DOX 140. VII — V.ECIMIB BEIECK III LIIE IIILETRALIULALAUPLUMUU | Box No. VII | Certain defects in the international | application |
|--|-------------|--------------------------------------|-------------|
|--|-------------|--------------------------------------|-------------|

The following defects in the form or contents of the international application have been noted:

Reference is in the description made to documents WO0008156, WO0008157 and WO0008158. However, it is assumed that the references instead should be WO0208156, WO0208157 and WO0208158.

Claims /PCT/FI2004/000713/ 16.01.2006

- 1. A method for the manufacture of a noble metal catalyst for hydrocarbon conversion, characterized in that the method comprises the following steps:
 - a) Pre-treatment of a support comprising a zeolite selected from medium and large pore zeolites having acid sites, at a temperature between 423 1173
 K, and optional modification of the support;
 - b) Deposition of a noble metal selected from platinum, palladium, ruthenium, rhodium, iridium and mixtures and combinations thereof by gas phase deposition technique comprising vaporisation of the noble metal precursor selected from β -diketonates and metallocenes and reaction with the support, and
 - c) Heat treatment at oxidising or reducing conditions.
 - 2. The method according to claim 1, characterized in that the noble metal is platinum.
 - 3. The method according to claim 1 or 2, characterized in that the zeolite is selected from large pore zeolites having weak or medium strength of acid sites.
 - 4. The method according to any one of claims 1 3, characterized in that the zeolite is selected from mesoporous aluminosilicates, crystalline aluminosilicates, crystalline aluminosphates and crystalline aluminosilicophosphates.
 - 5. The method according to any one of claims 1 4, characterized in that the zeolite is selected from MCM-41, Y- and beta-zeolites, mordenites, AlPO-5 and AlPO-11, SAPO-5 and SAPO-11.
 - 6. The method according to any one of claims 1 5, characterized in that the support further comprises inorganic oxide, carbon related material or mixtures or combinations thereof.
 - 7. The method according to claim 6, characterized in that the inorganic oxide is selected from silicon oxide, aluminum oxide, titanium oxide, zirconium oxide, tungsten oxide and magnesium oxide, preferably from silicon oxide and aluminum oxide.

- 8. The method according to claim 6, characterized in that the carbon related material is selected from activated carbon, graphite and carbon nanotubes.
- 9. The method according to any one of claims 1 8, characterized in that the noble metal precursor is (CH₃)₃(CH₃C₅H₄)Pt.
- 10. The method according to any one of claims 1 9, characterized in that the zeolite is MCM-41.
- 11. The method according to any one of claims 1 10, characterized in that in the first process step a) the support is pre-treated at a temperature of 423-1173 K, and in the second step b) the deposition is carried out in the presence of an inert carrier gas.
- 12. The method according to claim 11, characterized in that the inert carrier gas is nitrogen, helium, argon or methane.
- 13. The method according to any one of claims 1 12, **characterized** in that the modification in the first step a) is carried out by blocking part of available surface sites on the support with a blocking agent selected from alcohols, acetyl acetone, 2,2,6,6-tetramethyl-3,5-heptanedione, precursors of silicon oxide, aluminum oxide, titanium oxide, zirconium oxide, tungsten oxide and magnesium oxide, and nitrates.
- 14. The method according to claim 13, **characterized** in that the blocking agent is silicon tetrachloride, tetramethoxysilane, tetraethoxysilane, hexamethyldisilazane, hexamethyldisiloxane, aluminum chloride, aluminum ethoxide, aluminum (III) acetylacetonate, tris(2,2,6,6,-tetramethyl-3,5-heptanedionato)aluminum, trimethyl aluminum, triethyl aluminum, titanium tetrachloride, titanium isopropoxide, zirconium tetrachloride, tungsten oxychloride, tungsten hexachloride or tris(2,2,6,6-tetramethyl-3,5-heptanedionato) magnesium.
- 15. Use of the noble metal catalyst manufactured according to the method of any one of claims 1 14 in ring-opening, isomerisation, alkylation, hydrocarbon reforming, dry reforming, hydrogenation and dehydrogenation reactions, and preferably in ring-opening of naphthenic molecules.

16. A process for the manufacture of middle distillate diesel fuel, **characterized** in that a middle distillate feedstock is transferred to a reactor wherein it is allowed to react at a temperature of 283 - 673 K and under a pressure of 10 - 200 bar with hydrogen in the presence of a noble metal catalyst manufactured according to the method of any one of claims 1-14 to accomplish opening of naphthenes with two and multiple rings to produce isoparaffins, n-paraffins and mononaphthenes in the middle distillate region.